

# Tailoring Nanoadsorbent Surfaces for Recycling of LTM

Subjects: **Nanoscience & Nanotechnology**

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A series of adsorbents were tailored for selective extraction of rare earth elements (REE) and late transition metals (LTM) via grafting of ligands bearing specific N- and S-donor functions. All obtained adsorbents showed relatively quick uptake kinetics and high adsorption capacity 0.5 to 1.8 mmol/g, depending on the function and the target metal ion. The adsorption equilibrium data analyzed and fitted well to Langmuir isotherm model revealing monolayer adsorption process on homogeneously functionalized silica nanoparticles (NPs). Most of the employed ligands demonstrated higher affinity towards LTM compared to REE, related to the nature of the functional groups and their arrangement on the surface of nanoadsorbent.

recycling

silica nanoadsorbents

adsorption

REE

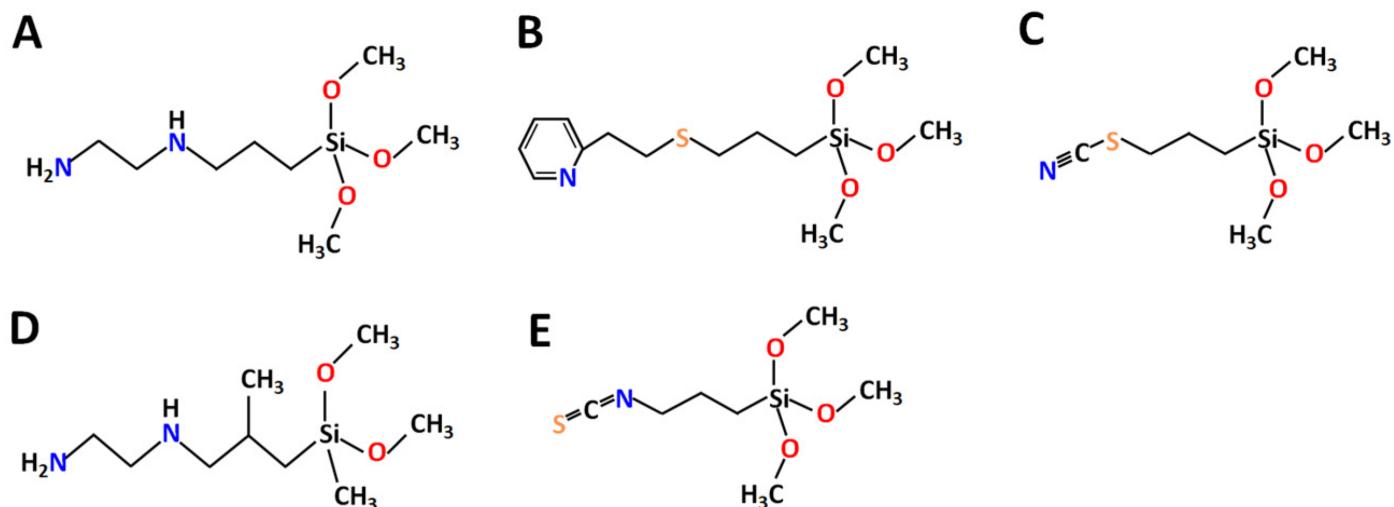
LTM

## 1. Introduction

During the past few decades, there has been a continuous increase in the applications of Rare Earth Elements (REE) and their alloys, making them critical elements for development of modern industries <sup>[1]</sup>. The main target markets using REEs include magnets, metallurgy, catalysts, polishing powders, batteries, mobile phones and other high-technology gadgets. With their growing demand and continuous supply risk, urban mining of REEs from different end-of-life products and industrial waste has gained increasing attention <sup>[2]</sup>. As such, permanent magnets, which have various applications in the development of new technological devices as well as for green energy production, are one of the most promising secondary sources of REEs that can be recycled and reused <sup>[3]</sup>. Common Rare Earth-based magnets include Neodymium–iron–boron (FeNdB) and Samarium–cobalt (SmCo) magnets <sup>[4]</sup>. One of the key challenges in the recycling of magnet materials lies in the need to separate REE from Late Transition Metals (LTM), which form their constituents or major materials of their casings <sup>[5]</sup>. The most common technology for REE separation is acidic leaching with different leaching agents such as hydrochloric and sulfuric acids <sup>[6][7]</sup>. Iron is the major component in FeNdB and in the casing of magnets in electronics. It needs to be removed in the step previous to the separation of all other components, for both economic and technical reasons. The well-established approaches for separation of iron from leachates include either precipitation of iron hydroxide during controlled elevation of pH <sup>[8]</sup> or the precipitation of all other components apart from iron by addition of oxalic acid and organic base <sup>[9]</sup>. The precipitate can then be calcined and re-dissolved in acid. Subsequent separation of the components can be achieved by solvent extraction, ion exchange, or adsorption <sup>[10]</sup>. Most of the established industrial methods require, however, repeated steps to obtain the desired purity, thus generating large amounts of hazardous and, in the case of primary ore treatment, even radioactive waste <sup>[11][12]</sup>. As an alternative to the

traditionally used methods, the application of solid-phase extraction (SPE) using nanosized functional adsorbents has been proven to be an effective and more environmentally friendly method for REE recovery [13]. Various types of nanosorbents have been synthesized for SPE recovery of REEs [14][15][16][17][18][19][20][21]. Several reviews have already been devoted to the discussion of the advantages and challenges in the application of functional solid adsorbents for REE separation [22][23]. Recent works have shown that organic–inorganic functionalized silica nanoparticles possess great adsorption capacity and selectivity towards many metal ions, including heavy metals and REEs [24]. Functional groups such as iminodiacetic acid (IDA), diethylenetriaminepentaacetic acid (DTPA), ethylenediaminetetraacetic acid (EDTA) and triethylenetetraminehexaacetic acid (TTHA) were grafted on dense  $\text{SiO}_2$  nanoparticles as well as  $\text{SiO}_2$  core–shell magnetic nanoparticles and tested for different REEs adsorption and separation. High adsorption capacities of up to 300 mg of  $\text{RE}^{3+}/\text{g}$  were reached, and distinct selectivity trends towards different REEs depending on the complexonate [25][26][27].

The majority of earlier successfully applied ligands belonged to the classes of either complexons, i.e., amino carboxylic acids [28], or crown ethers/cyclenes. These types of ligands revealed strong affinity to both REE and LTM. In this entry, the new ligands (N-(2-Aminoethyl)-3-aminopropyltrimethoxysilane **L1** and N-(2-Aminoethyl)-3-Aminolsobutylmethyl Dimethoxysilane **L4**—a derivative of ethylene diamine, known for high affinity to  $\text{Ni}^{2+}$  and  $\text{Cu}^{2+}$  and, to a lesser extent, for  $\text{Co}^{2+}$  [29][30][31]; 2-(2-Pyridilethyl) Thiopropyltrimethoxysilane **L2**—a derivative of pyridine with potentially good affinity to LTM and also a sulfur bridge [32][33]; and Triethoxy(3-isothiocyanatopropyl)silane **L3** and Triethoxy(3-thiocyanatopropyl)silane **L5**—derived from isothiocyanate with potential affinity to  $\text{Ni}^{2+}$  and  $\text{Co}^{2+}$  [34], were selected and grafted on  $\text{SiO}_2$  nanoparticles to achieve selectivity for separating LTM from REEs in mixed solutions (**Figure 1**).

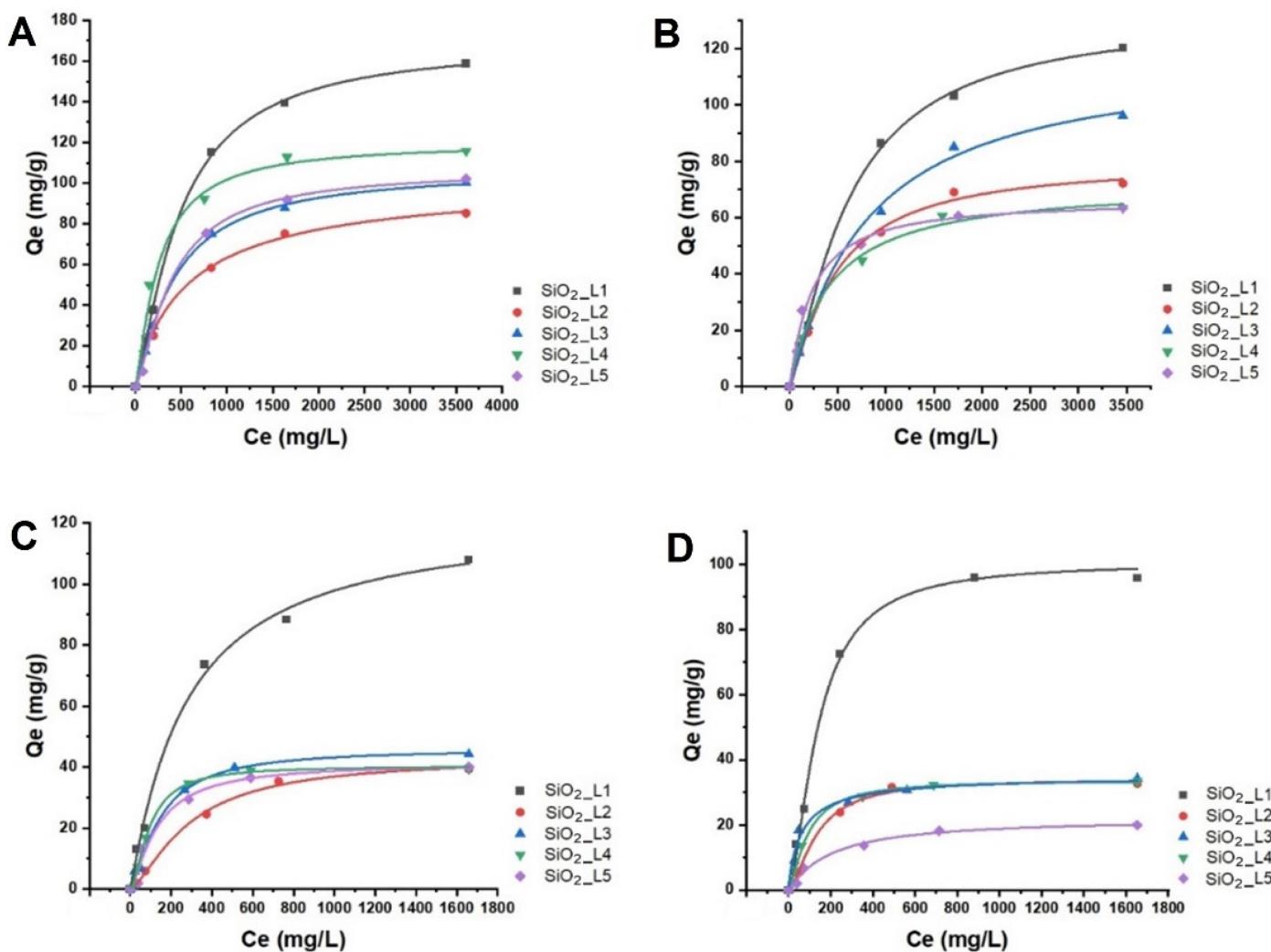


**Figure 1.** Chemical structure of selected ligands: (A) **L1**, (B) **L2**, (C) **L3**, (D) **L4** and (E) **L5**.

## 2. Adsorption Equilibrium Isotherms

The effect of the concentrations of LTM (Co and Ni) and of  $\text{RE}^{3+}$  (Nd and Sm) on adsorption efficiency was investigated in batch studies at room temperature. The results showed that the adsorbed amount of metal ions on

grafted  $\text{SiO}_2$  NPs increased with increasing the initial metal concentration and reached to the maximum adsorption capacity at higher concentrations due to saturation of the binding sites (**Figure 2**). The maximum adsorption capacities are summarized in **Table 1**. Based on the results, **SiO<sub>2</sub>\_L1** demonstrated higher adsorption capacities for all LTM and REEs, which is in agreement with TGA results, considering the grafted amount of the ligands per unit mass of  $\text{SiO}_2$  NPs was higher compared to **SiO<sub>2</sub>\_L2** and **SiO<sub>2</sub>\_L3**.  $\text{SiO}_2$  with both **L2** and with **L3** had similar maximum adsorption capacities for most of the metal ions, only for Co adsorption did  $\text{SiO}_2$  NPs grafted with **L3** ligands demonstrate a slightly higher adsorption capacity. However, acid-treated  $\text{SiO}_2$  with **L3** (**SiO<sub>2</sub>\_L3\_acid**) and **L5** (**SiO<sub>2</sub>\_L5\_acid**) showed improved adsorption by increasing their maximum capacities by twice for Co, Nd, Sm, and by almost five times in the case of Ni. According to the literature, sulfur- and amine-containing groups possess higher selectivity towards LTM, which can explain the higher adsorption capacities towards Ni and Co for most of these ligands [35][36][37][38][39][40].



**Figure 2.** Langmuir adsorption isotherms of (A) Sm, (B) Nd, (C) Co and (D) Ni ions onto functionalized silica nanoparticles.

**Table 1.** Maximum adsorption capacities of grafted  $\text{SiO}_2$  NPs towards REEs and LTM.

Sample	Ni (mmol/g)	Co (mmol/g)	Nd (mmol/g)	Sm (mmol/g)
SiO <sub>2</sub> _L1	1.66	1.83	0.83	1.10
SiO <sub>2</sub> _L2	0.55	0.66	0.50	0.56
SiO <sub>2</sub> _L3	0.58	0.75	0.67	0.66
SiO <sub>2</sub> _L4	0.57	0.67	0.44	0.77
SiO <sub>2</sub> _L5	0.34	0.68	0.44	0.68
SiO <sub>2</sub> _L3_acid	1.00	1.33	0.75	0.83
SiO <sub>2</sub> _L5_acid	1.66	1.33	0.75	1.00

**References** adsorbents have previously been tested for REE and LTM removal from aqueous solutions. **Table 2** summarizes various results with silica-based and other adsorbent materials for their maximum uptake capacity. It can be noted that SiO<sub>2</sub>-Ln nanoparticles present a competitive performance for the binding of selected metals. Some materials have significantly high sorption properties; however, in most cases, the maximum uptake capacities are lower than the values reported for the Chinese policies on rare earth supply chain resilience. *Resour. Conserv. Recycl.* 2019, **142**, 101–112.

**Table 2.** Maximum adsorption capacities of different adsorbents towards REEs and LTM.

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Adsorbent	Metal	Uptake (mmol/g)	References <sup>net</sup>
Phosphorus functionalized adsorbent	Nd(III)	1.13	[41]
DETA-functionalized chitosan magnetic nano-based particles	Nd(III)	0.35	[42]
Zr modified mesoporous silica SBA-15	Sm(III)	0.28	[43]
Silica/polyvinyl imidazole/H <sub>2</sub> PO <sub>4</sub> -core-shell NPs	Sm(III)	1.04	[44]
Cyclen-functionalized ethylene-based mesoporous organosilica NPs	Ni(II)	3.94	[14]
Cyclen-functionalized ethylene-based mesoporous organosilica NPs	Co(II)	3.84	[14]
Ni(II) ion-imprinted silica gel polymer	Ni(II)	0.35	[45]

for neodymium recovery from scrap Nd-Fe-B magnet. *Metall. Mater. Trans. A Phys. Metall. Mater. Sci.* 2013, **44**, 5825–5833. It has to be mentioned that selective separation of REE from LTM by functional nanoadsorbents has so far not been addressed in the literature.

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The adsorption kinetics showed that most of the uptake (60–80%) occurred within the first 1–2 h of interaction of metals with silica nanoparticles. Slow adsorption continues, and equilibrium is reached after 3–5 h (Figure 3) and Characterization of Poly(pyrrole-1-carboxylic acid) for Preconcentration and Determination of Rare Earth Elements and Heavy Metals in Water Matrices. *ACS Appl. Mater. Interfaces* 2021, 13, 34782–34792.

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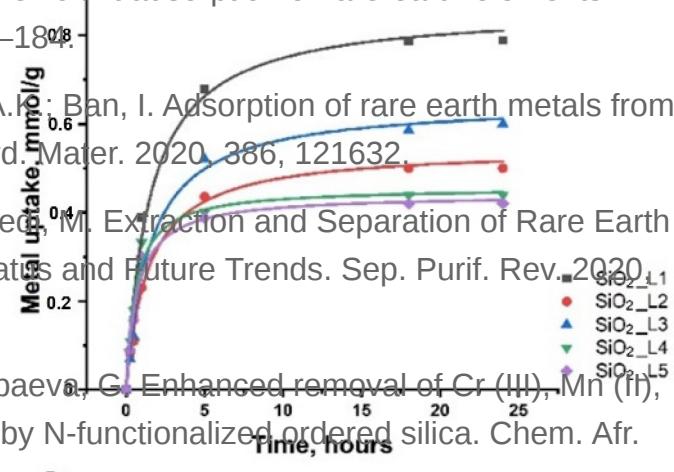
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**Table 3.** Molar ratios of Co and Ni against Sm and Nd by EDS analysis.

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Sample	Ni/Nd	Co/Sm	Ni/Co
$\text{SiO}_2\text{-L1}$	5.1:1	1:1.65	3.5:1
$\text{SiO}_2\text{-L2}$	1:1.78	1:12	1.6:1
$\text{SiO}_2\text{-L3}$	1:1	1:18	1:1
$\text{SiO}_2\text{-L4}$	1.33:1	1:18	1.85:1
$\text{SiO}_2\text{-L5}$	1:3	1:1	1.85:1
$\text{SiO}_2\text{-L3_acid}$	1:2.5	6:1	1.3:1
$\text{SiO}_2\text{-L5_acid}$	15:1	6:1	2.75:1

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